

## Energy, Work, and Heat

- Consider energy and molecules.
  - Energy affects how molecules react. In particular the distribution of energy within a molecule influences how it behaves both chemically and physically.
- How do molecules have energy?
  - In chemical bonds. The more energy required to break a bond, the stronger the bond is.
  - In internal motions (such as vibration and rotation) and electronic excitations.
  - As kinetic energy of motion. Temperature is a way of measuring the average kinetic energy of a system of molecules at equilibrium.

### Energy (from a Thermodynamic Perspective)

- Consider the exothermicity of a chemical reaction.
  - Food Calories
  - Fuel Combustion

- Corrosion
- Decomposition
- Energy is considered on a scale related to changes, not an absolute scale.
- In thermodynamics, two particular forms of energy are considered:
  - $q$  heat
  - $w$  work

## What is energy?

- What are the properties of energy?
  - Cannot be created or destroyed
  - Can only change form such as be converted to heat, work, or internal energy.

## First Law of Thermodynamics

- Energy is conserved.
- Energy is not created or destroyed.

## **What are “Laws of Thermodynamics”?**

- The ”Laws of Thermodynamics” are a set of postulates from which theorems and other relationships may be derived.

## **The transfer of energy called work**

- Work is only associated with the performance of a thermodynamic process.
- Some ”types” of work:
  - mechanical
  - electrical
  - magnetic
  - gravitational
  - surface
- In this chapter, work will usually be in the form of mechanical work being done by or on a system.
- What is a system?

## Systems

- Open - transfers mass and energy to and from the surroundings.
- Closed - does not transfer mass to or from the surroundings.
- Isolated - transfers neither mass or energy to or from the surroundings.

## Surroundings

- Since we are dealing with equilibrium thermodynamics, the state variables describing the surroundings may be of interest.
  - For example, consider the temperature of a constant temperature bath. A process carried out at constant temperature is isothermal.

## The variation of work with the path

- Work is a path function.

- How the work is done matters.

$$\text{work} = \int_{\text{path}} \mathbf{F}(\mathbf{r}) \cdot d\mathbf{r}$$

- $\mathbf{F}(\mathbf{r})$  is the force vector which varies with  $\mathbf{r}$
- Both force and displacement have the same direction.
- Consider pressure volume work:
  - Ideal gas at  $P_i = 1$  atm confined in cylinder of volume  $V_i$  by a piston of area  $A$ .
  - This ideal piston at  $x = x_0$  has no mass, no friction, and does not leak.
  - Surroundings include a constant temperature bath at temperature  $T_i$ .
  - Drop a brick on the piston, instantaneously increasing the pressure to  $P_f$

### **How much work is done?**

- Consider:
  - What is the force?
  - What is the displacement?

- The force is:

$$P_{ext} = P_i + \frac{Mg}{A}$$

or

$$F(x) = P_i A + Mg$$

- Note that  $F(x)$  in this case is a constant independent of position.
- Note that the direction of the force is downward, thus there is a negative sign since the  $x$  axis is positive upward.
- The displacement is the distance  $h$ , which the distance that the piston moved down when the brick was dropped on it.
  - The initial position of the piston is  $x_0$ .
  - The final position is  $x_0 - h$ .
- Therefore the work is:

$$\begin{aligned} w &= \int_{path} \mathbf{F}(\mathbf{r}) \cdot d\mathbf{r} = - \int_{path} F(x) dx \\ &= - \int_{x_0}^{x_0-h} (P_i A + Mg) dx \\ &= - (P_i A + Mg) \int_{x_0}^{x_0-h} dx \end{aligned}$$

$$= - (P_i A + Mg) (-h)$$

$$w = (P_i A + Mg) h$$

- The volume change during this process is:

$$\Delta V = V_f - V_i = A(x_0 - h) - Ax_0 = -Ah$$

- Therefore:

$$w = - \left( P_i + \frac{Mg}{A} \right) \Delta V = -P_{ext} \Delta V$$

## Thermodynamic Sign Convention for Work

- Work is positive when work is done on the system.
- Work is negative when work is done by the system.
- The magnitude of work can be considered as the area in PV space under the curve representing the path.
  - This area will vary with the path, which is consistent with work being a path function.

- Consider now some different paths from  $(P_i, V_i)$  to  $(P_f, V_f)$ . Recall that the process is isothermal since there is a constant temperature bath as surroundings.
  - Path 1: Break the brick in half and change the pressure in two steps.
  - Path 2: Crumble the brick to dust and change the pressure in very small increments by adding the dust one grain at a time.
- Which path gives the minimum amount of work to be done on the system?

## Reversible Isothermal Work

- If the work is carried out in infinitesimal steps infinitely slowly, then the process is quasi-static.
- For such a process, deviations from equilibrium are infinitesimal.
- Therefore all points on the path may be described by the equation of state for the system.



- Consider an ideal gas undergoing reversible, isothermal expansion from  $(P_i, V_i)$  to  $(P_f, V_f)$ . Therefore:

$$w = - \int_{V_i}^{V_f} P_{sys}(V) dV = -nRT \int_{V_i}^{V_f} \frac{dV}{V}$$

$$= -nRT \ln \left( \frac{V_f}{V_i} \right)$$

- If the process is a compression (i.e.  $V_f$  smaller than  $V_i$ ), work is positive and work is done on the system.
- If the process is an expansion (i.e.  $V_f$  larger than  $V_i$ ), work is negative and work is done by the system.
- Now consider a cyclic process.
  - First the gas is compressed isothermally at  $P_f$  from  $V_i$  to  $V_f$ .
  - Then the gas is expanded at  $P_i$  from  $V_f$  to  $V_i$ .
  - Therefore there is no overall change in state.

- What is the work done by or on the system over this path?
- What if the path were followed in the opposite direction?

### **The Transfer of Energy called Heat**

- Consider the compression of a gas.
- What would happen if, instead of carrying out this process in a closed system in contact with a constant temperature bath, the process were carried out in an isolated system?
  - Would the temperature stay constant?  
Why or why not?
  - Compared to the isothermal reversible path, would more or less work be done on the system?

### **What is the Thermodynamic Definition of Temperature?**

- Consider an ideal gas at reference temperature. This reference temperature has to be readily accessible experimentally. The triple point of water is convenient. By definition, the temperature is 273.16 K.

- Consider the PV product of any real gas at this temperature. Then the temperature can be defined as:

$$\frac{T}{273.16} = \lim_{P \rightarrow 0} \frac{(PV)_T}{(PV)_{273.16}}$$

- Consider the compression of an isolated system.
  - Will the (PV) product be higher or lower than that for a reversible isothermal compression starting at the same pressure and volume and going to the same final volume?
- When work is done by or on an isolated system, the process is called *adiabatic*.
  - In an adiabatic process no energy has been exchanged with the surroundings.
- Adiabatic work from a particular starting point to a particular final point is independent of the path.
  - Therefore adiabatic work must be a state function.

## Internal Energy

- Internal energy is symbolized by  $U$ .
- Defined with respect to work done on an adiabatic path.

$$\Delta U = U_f - U_i = \int_{U_i}^{U_f} dU = \int_{\text{adiabatic path}} dw = w_{ad}$$

- Can we get to any state  $(P_f, V_f)$  on an adiabatic path?
  - Not all final states can be reached by an adiabatic path.
  - But if  $U$  is a state function, we need to be able to define  $\Delta U$  for the change from any initial state to any final state. Therefore we must consider other types of processes, which can involve the transfer of heat.
- Heat is any form of energy transferred by a process other than work.
  - Recall that heat  $q$  is a path function.
- Consider heat along a path at constant volume.
  - Consider a gas cylinder with the piston fixed in position.

- Apply a source of energy.
- The temperature will rise.
- This path does not involve work.
- For heat at constant volume, no work is done since  $\Delta V = 0$ .

$$\begin{aligned}\Delta U_V &= U_f - U_i = \int_{U_i}^{U_f} dU \\ &= \int_{\text{constant volume path}} dq = q_V\end{aligned}$$

- Therefore constant volume heat  $q_V$  is equivalent to the change in the state function internal energy ( $\Delta U_V$ ).

## **Thermodynamic sign convention for heat**

- Heat is positive when energy is transferred to the system from the surroundings.
- Heat is negative when energy is transferred from the system to the surroundings.

- Internal energy of a system changes due to the additive effects of heat and work associated with a thermodynamic process:

$$dU = dq + dw$$

or in integrated form:

$$\Delta U = \int_{path} dq + \int_{path} dw$$

## Cycles

- Associated with a cycle:
  - What would be  $\Delta U$ ?
  - What would be the work?
  - What would be the heat?

## Simple Consequences of the First Law

- The transfer of heat alone often results in a change in temperature with the change in temperature being proportional to the heat transferred:

$$dq = CdT$$

- The proportionality factor,  $C$  is the heat capacity, which depends on the materials constituting the system and on the path of the process.
  - $C_V$  is associated with a constant volume path.
  - $C_P$  is associated with a constant pressure path.
- For an ideal gas statistical mechanics shows:

$$C_V = \frac{3}{2}nR \quad \text{or} \quad \frac{\overline{C}_V}{R} = \frac{C_V}{nR} = \frac{3}{2}$$

$$C_P = \frac{5}{2}nR \quad \text{or} \quad \frac{\overline{C}_P}{R} = \frac{C_P}{nR} = \frac{5}{2}$$

- Combined with our earlier expression for  $\Delta U$ , we get:

$$\begin{aligned} \Delta U &= \int_{path} dq + \int_{path} dw \\ &= \int_{path} C_{path} dT - \int_{path} P_{ext} dV \end{aligned}$$

- The expression for  $\Delta U$  indicates that  $U$  varies with  $T$  and  $V$ , i.e.  $U = U(T, V)$ .

$$dU = \left( \frac{\partial U}{\partial T} \right)_V dT + \left( \frac{\partial U}{\partial V} \right)_T dV$$

Therefore:

$$dU = C_{path} dT - P_{ext} dV$$

- If  $\Delta V = 0$  then:

$$dU_V = \left( \frac{\partial U}{\partial T} \right)_V dT$$

$$dU_V = C_V dT$$

Therefore:

$$\left( \frac{\partial U}{\partial T} \right)_V = C_V$$

- Suppose  $dT = 0$ . Then:

$$dU = \left( \frac{\partial U}{\partial V} \right)_T dV$$



but

$$dU = C_{path} dT - P_{ext} dV$$

retains both terms, since in order for  $C_{path} dT$  to be zero, the path must be adiabatic and both  $T$  and  $V$  change on an adiabatic path.

## The Joule Expansion

- What about  $(\partial U/\partial V)_T$ ?
- Joule did some experiments to attempt to measure it. See Fig. 2.6.
  - Constant temperature maintained by a water bath.
  - Two chamber vessel
  - Volume of both chambers known
  - One chamber at high  $P$
  - Other chamber at  $P_{ext} \approx 0$
  - Chambers separated by stopcock
- Stopcock opened, gas expands against  $P_{ext} \approx 0$ 
  - Therefore no work done
  - No temperature change observed.

- Problems with experimental design:
  - Temperature change may have been too small to observe.
  - Make the system bigger
  - Make the water bath smaller
- BUT conclusion is valid.
  - Rigorously for an ideal gas:

$$\left(\frac{\partial U}{\partial V}\right)_T = 0$$

- In the low pressure limit for a real gas:

$$\lim_{P \rightarrow 0} \left(\frac{\partial U}{\partial V}\right)_T = 0$$

## General Adiabatic Processes

- Consider an adiabatic process.
  - Along the path of this process  $dq = 0$ .
  - Therefore  $CdT = 0$ , even though  $dT \neq 0$ .
  - Therefore  $C_{ad} = 0$ .
- For this path

$$dU_{ad} = -P_{ext}dV = dw_{ad}$$

- But for any path:

$$dU = \left( \frac{\partial U}{\partial T} \right)_V dT + \left( \frac{\partial U}{\partial V} \right)_T dV$$

- We have already shown for an ideal gas that:

$$\left( \frac{\partial U}{\partial V} \right)_T = 0$$

Therefore, for an ideal gas:

$$dU = \left( \frac{\partial U}{\partial T} \right)_V dT = C_v dT = \frac{3}{2} n R dT$$

- Thus:

$$\int dU_{ad} = \Delta U_{ad} = w_{ad} = \int C_v dT = \frac{3}{2} n R \Delta T$$

- Consider an adiabatic process with constant  $P_{ext}$ :

$$w_{ad} = -P_{ext} \Delta V$$

- With the previous equation this gives:

$$\Delta T = -P_{ext} \frac{\Delta V}{C_v} = -\frac{2}{3} \frac{P_{ext} \Delta V}{n R}$$

- Consider adiabatic expansion against zero external pressure  $P_{ext} = 0$ :
  - Then  $w_{ad} = 0$ ,  $\Delta T = 0$  and this is the Joule experiment run adiabatically.
- Consider an adiabatic process with constant  $P_{ext}$ :

$$w_{ad} = -P_{ext}\Delta V$$

$$\Delta T = -P_{ext} \frac{\Delta V}{C_v} = -\frac{2}{3} \frac{P_{ext}\Delta V}{nR}$$

- If  $\Delta V$  is negative, a compression has occurred and  $w_{ad}$  and  $\Delta T$  are positive.
  - If  $\Delta V$  is positive, an expansion has occurred and  $w_{ad}$  and  $\Delta T$  are negative.
- When  $w_{ad}$  is positive, energy has been put into the system.
  - Since the process is adiabatic, energy cannot escape as heat.
  - Therefore a temperature change occurs, the magnitude of which is controlled by the heat capacity.

## Adiabatic Reversible Processes in an Ideal Gas

- Assume an ideal gas, therefore  $PV = nRT$
- Reversible, therefore  $P_{ext} = P_{sys} + dP$
- Adiabatic, therefore  $dq = 0$ .
- At all points of this path:

$$dU = dw_{ad}$$

$$C_V dT = -P_{sys} dV = \frac{-nRT}{V} dV$$

Therefore:

$$C_V \frac{dT}{T} = -nR \frac{dV}{V}$$

Integration over the path yields:

$$\int_{T_i}^{T_f} C_V \frac{dT}{T} = \int_{V_i}^{V_f} -nR \frac{dV}{V}$$

$$C_V \int_{T_i}^{T_f} \frac{dT}{T} = -nR \int_{V_i}^{V_f} \frac{dV}{V}$$

$$C_V \ln \left( \frac{T_f}{T_i} \right) = -nR \ln \left( \frac{V_f}{V_i} \right)$$

- Recall for an ideal gas that  $C_V = 3nR/2$ . Thus:

$$\frac{3}{2}nR \ln \left( \frac{T_f}{T_i} \right) = -nR \ln \left( \frac{V_f}{V_i} \right)$$

- Dividing through by  $nR$  and recognizing that  $\ln(1/x) = -\ln x$  gives:

$$\frac{3}{2} \ln \left( \frac{T_f}{T_i} \right) = -\ln \left( \frac{V_f}{V_i} \right) = \ln \left( \frac{V_i}{V_f} \right)$$

- Dividing through by  $3/2$  and recognizing that  $a \ln x = \ln x^a$  gives:

$$\ln \left( \frac{T_f}{T_i} \right) = \frac{2}{3} \ln \left( \frac{V_i}{V_f} \right) = \ln \left( \frac{V_i}{V_f} \right)^{2/3}$$

or

$$T_f = T_i \left( \frac{V_i}{V_f} \right)^{2/3}$$

- We now have an equation to describe our reversible adiabatic path for an ideal gas.

$$T_i V_i^{2/3} = T_f V_f^{2/3}$$

- If  $T$  and  $V$  are known and since the equation of state holds along a reversible path, then  $P$  can be determined.
- Substituting  $PV/nR$  for  $T$  gives:

$$\left( \frac{P_i V_i}{nR} \right) V_i^{2/3} = \left( \frac{P_f V_f}{nR} \right) V_f^{2/3}$$

- Factoring out  $nR$  on both sides gives:

$$P_i V_i^{5/3} = P_f V_f^{5/3}$$

or

$$P V^{5/3} = \text{constant}$$

- The factor  $5/3$  is usually represented as  $\gamma$  can be shown to originate from  $(C_V + nR)/C_V$ .
- But  $C_P = C_V + nR$ , thus

$$\gamma = \frac{C_P}{C_V}$$

and

$$PV^\gamma = \text{constant}$$

$$TV^{\gamma-1} = \text{constant}$$

- Similarly, substituting  $nRT/P$  for  $V$  gives a relation between  $T$  and  $P$ :

$$T_i \left( \frac{nRT_i}{P_i} \right)^{\gamma-1} = T_f \left( \frac{nRT_f}{P_f} \right)^{\gamma-1}$$

$$\frac{T_i^\gamma}{P_i^{\gamma-1}} = \frac{T_f^\gamma}{P_f^{\gamma-1}}$$

$$\frac{T_i^{\gamma/(\gamma-1)}}{P_i} = \frac{T_f^{\gamma/(\gamma-1)}}{P_f}$$

## Paths Equivalent to an Adiabatic Path

- Referring to Figure 2.7 on page 50 of Winn, consider the adiabatic reversible path I between an initial state  $(P_i, V_i)$  and final state  $(P_f, V_f)$  of an ideal gas.
  - We wish to determine  $\Delta U_I$  associated with this change.
- Since  $U$  is a state function, we can construct any alternate path we deem convenient.
  - An especially convenient path consists of a path II from  $(P_i, V_i)$  to final  $V_f$  along an



isotherm, followed by path III along an isochore (constant volume) to  $(P_f, V_f)$ .

- These path segments are especially convenient because it is very easy to determine  $\Delta U_{II}$  and  $\Delta U_{III}$ .
- For the any isothermal change in state of an ideal gas, there is no change in  $U$ . Therefore  $\Delta U_{II} = 0$ .
- For a constant volume change in an ideal gas, the change in  $U$  is determined by the constant volume heat capacity and the temperature change. Therefore:

$$\Delta U_{III} = C_V(T_f - T_i)$$

Thus:

$$\Delta U_I = \Delta U_{II} + \Delta U_{III} = 0 + C_V (T_f - T_i)$$

## Closer Look at the Meaning of Adiabaticity

- A real process approaches adiabaticity if it is carried out sufficiently quickly that the process is over before heat has had a chance to transfer to or from the surroundings.
- Examples:
- Expansion of compressed gas from a cylinder.
  - The valve can be observed to "ice" up.
- Air masses in meteorology.
  - As air rises, it cools adiabatically since air itself does not transfer heat readily.
  - If the air mass was not dry, this cooling can lead to precipitation.

## A New State Function, Enthalpy

- Constant pressure conditions are encountered far more frequently than constant volume conditions.
  - We already have  $C_p$  which is the heat capacity along a path of constant pressure.

- Recall  $dq_p = C_p dT$ .
- Enthalpy is to constant pressure conditions what internal energy is to constant volume conditions.
- Consider  $U + PV$ . The corresponding total differential is:

$$\begin{aligned} d(U + PV) &= dU + PdV + VdP \\ &= dq - P_{ext}dV + PdV + VdP \end{aligned}$$

- At constant pressure,  $dP = 0$  and  $P = P_{ext}$ . Therefore:

$$d(U + PV) = dq - P_{ext}dV + P_{ext}dV + VdP$$

$$d(U + PV)_P = dq_P$$

$$H \equiv U + PV$$

Consequently,

$$dH_P = dq_P = C_P dT$$

and:

$$\left( \frac{\partial H}{\partial T} \right)_P = C_p$$

- If an ideal gas is under consideration, then

$$PV = nRT$$

and

$$H(\text{ideal gas}) = U(\text{ideal gas}) + PV$$

or

$$H = U + nRT.$$

- In differential form this becomes:

$$dH = dU + nRdT$$

or:

$$C_P dT = C_V dT + nRdT$$

Thus:

$$C_P - C_V = nR$$

for an ideal gas.

- Although  $H(P, T)$  has been defined with regard to constant pressure processes, it is a state function.

- Therefore  $\Delta H$  can be calculated for any change regardless of path followed by the process.

$$\begin{aligned} dH &= \left( \frac{\partial H}{\partial T} \right)_P dT + \left( \frac{\partial H}{\partial P} \right)_T dP \\ &= C_P dT + \left( \frac{\partial H}{\partial P} \right)_T dP \end{aligned}$$

- Now consider  $(\partial H / \partial T)_V$ :

$$\left( \frac{\partial H}{\partial T} \right)_V = C_P + \left( \frac{\partial H}{\partial P} \right)_T \left( \frac{\partial P}{\partial T} \right)_V$$

- What about  $(\partial H / \partial T)_P$ ?
- Recall the cyclic rule:

$$-1 = \left( \frac{\partial H}{\partial T} \right)_P \left( \frac{\partial T}{\partial P} \right)_H \left( \frac{\partial P}{\partial H} \right)_T$$

- Thus:

$$\begin{aligned} \left( \frac{\partial H}{\partial P} \right)_T &= - \left( \frac{\partial H}{\partial T} \right)_P \left( \frac{\partial T}{\partial P} \right)_H \\ \left( \frac{\partial H}{\partial P} \right)_T &= -C_P \left( \frac{\partial T}{\partial P} \right)_H \end{aligned}$$

(A process during which  $dH = 0$  is an isenthalp.)

- Therefore:

$$\begin{aligned}\left(\frac{\partial H}{\partial T}\right)_V &= C_P - C_P \left(\frac{\partial T}{\partial P}\right)_H \left(\frac{\partial P}{\partial T}\right)_V \\ &= C_P \left[1 - \left(\frac{\partial T}{\partial P}\right)_H \left(\frac{\partial P}{\partial T}\right)_V\right]\end{aligned}$$

- How is  $(\partial T/\partial P)_H$  evaluated?

### **The Joule-Thomson Effect (Fig 2.8)**

- Joule and Thomson devised an experiment that involved constant enthalpy.
  - Apparatus is insulated, therefore the process is adiabatic.
  - Two pistons and a porous wall.
  - Start with all the gas on left side of the wall at  $(P_i, V_i, T_i)$ .
  - Push the gas through the porous wall with the left piston, while at the same time withdrawing the right piston, so as to maintain constant pressure.

- Reach final state with the gas to the right side of the wall at  $(P_f, V_f, T_f)$ .
- Adiabatic, therefore  $q = 0$ . Thus:

$$\Delta U = w_{ad}$$

- The work must be considered in two parts.
  - The gas is compressed by the first piston to the barrier.
  - The work associated with this is  $P_i V_i$ , since the gas is compressed at constant  $P_i$  from  $V_i$  to zero.
  - The gas is expanded by the second piston at  $P_f$  from zero to  $V_f$ .
  - Therefore  $-P_f V_f$  is the work associated with this.
  - Thus  $w_{ad} = P_i V_i - P_f V_f = \Delta U$ .
  - But  $\Delta U = U_f - U_i$ .
  - Therefore:

$$U_i + P_i V_i = U_f + P_f V_f$$

$$H_i = H_f$$

- Since  $\Delta H = 0$ , the process is isenthalpic.

- Final temperature is measured at various final pressures for the same initial pressure and temperature.
  - The result is a temperature pressure isenthalp.
  - The slope of this  $(\partial T / \partial P)_H$  is the Joule-Thompson coefficient:

$$\mu_{JT}(T, P) = \left( \frac{\partial T}{\partial P} \right)_H$$

- $\mu_{JT}(T, P) = 0$  for an ideal gas.
  - The deviation of  $\mu_{JT}(T, P)$  from zero contains information about the nonideal behaviour of the gas.
- In chapter 3, it will be shown that:

$$\mu_{JT}(T, P) = \frac{1}{C_P} \left[ T \left( \frac{\partial V}{\partial T} \right)_P - V \right]$$

- Recall the virial equation of state, through to the second virial coefficient:

$$\frac{P\bar{V}}{RT} = 1 + \frac{B(T)}{\bar{V}}$$



- This can be rearranged to:

$$\frac{RT}{P\bar{V}} = \frac{1}{1 + \frac{B(T)}{\bar{V}}}$$

- If  $\bar{V} \gg B$ , then this becomes:

$$\frac{RT}{P\bar{V}} = 1 - \frac{B(T)}{\bar{V}}$$

- Multiplying through by  $\bar{V}$  gives:

$$\frac{RT}{P} = \bar{V} - B(T)$$

or

$$\bar{V} = \frac{RT}{P} + B(T)$$

- Therefore:

$$\left(\frac{\partial V}{\partial T}\right)_P = \frac{R}{P} + \left(\frac{\partial B}{\partial T}\right)_P$$

- Substituting this into the expression for  $\mu_{JT}$  yields:

$$\mu_{JT}(T, P) = \frac{1}{C_P} \left[ T \left(\frac{\partial B}{\partial T}\right)_P - B \right]$$

- When  $B = T(\partial B/\partial T)_P$ , then  $\mu_{JT} = 0$ . The temperature at which that occurs is the Joule-Thomson inversion temperature,  $T_I$ .
- Recall that for the van der Waals virial expression,

$$B(T) = b - \frac{a}{RT}$$

- Then at  $T_I$ ,

$$b - \frac{a}{RT_I} = T_I \left( \frac{a}{RT_I^2} \right)$$

and

$$T_I = 2 \left( \frac{a}{Rb} \right) = 2T_B$$

- Below  $T_I$  gases cool when expanded.
- Above  $T_I$  gases warm up when expanded.
- Real gases exhibit a range of inversion temperatures that depend on initial pressure.
  - The van der Waals equation of state predicts:

$$\tilde{P} = \left[ 3 \left( \frac{\tilde{T}}{2} \right)^{1/2} - 1 \right] \left[ 1 - \left( \frac{\tilde{T}}{2} \right)^{1/2} \right]$$

- Recall

$$\left(\frac{\partial H}{\partial P}\right)_T = -C_P \left(\frac{\partial T}{\partial P}\right)_H$$

Then

$$\left(\frac{\partial H}{\partial P}\right)_T = -C_P \mu_{JT}$$

- Recall also:

$$\begin{aligned} \left(\frac{\partial H}{\partial T}\right)_V &= C_P - C_P \left(\frac{\partial T}{\partial P}\right)_H \left(\frac{\partial P}{\partial T}\right)_V \\ &= C_P \left[1 - \left(\frac{\partial T}{\partial P}\right)_H \left(\frac{\partial P}{\partial T}\right)_V\right] \end{aligned}$$

This becomes:

$$\left(\frac{\partial H}{\partial T}\right)_V = C_P \left[1 - \mu_{JT} \left(\frac{\partial P}{\partial T}\right)_V\right]$$

- The differential is:

$$dH = \left(\frac{\partial H}{\partial T}\right)_P dT + \left(\frac{\partial H}{\partial P}\right)_T dP$$

which becomes:

$$dH = C_P dT - C_P \mu_{JT} dP$$